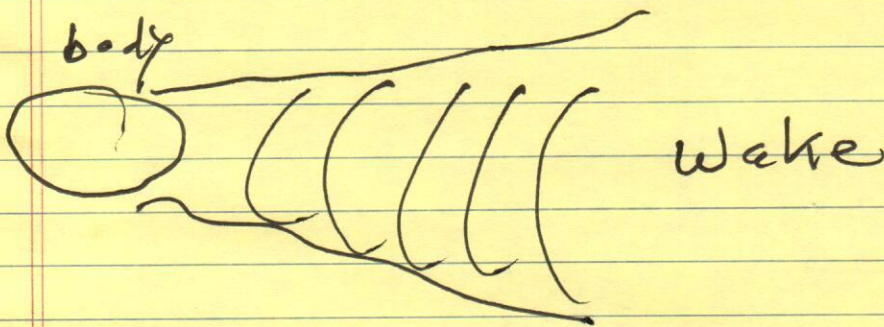


B.) Wakes - Simple physics

cf: { Prandtl -  
Tietjens,  
Falkovich,  
Lander

Wake is:

- region of departure from potential flow behind object moving thru water and experiencing drag



→ wake is inextricably coupled to drag

- Message of wakes:

A little  $\nu$  forces a global adjustment in flow structure

- drag - thinking in frame where object at rest, drag results from loss of flow momentum to object



→ wake is region of flow where loss of momentum is evident.

c.e.

- if potential flow (no drag)



symmetry  
upstream downstream  
in  $\perp$  displacement  
of fluid element

- with no-slip b.c., viscosity, turbulence etc.

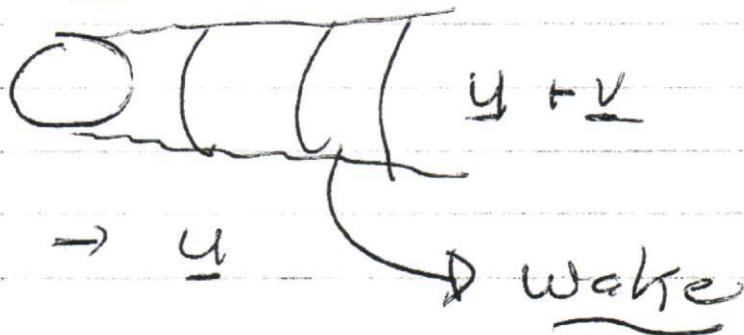
$\vec{u}$

$\vec{u}$

→

→

→

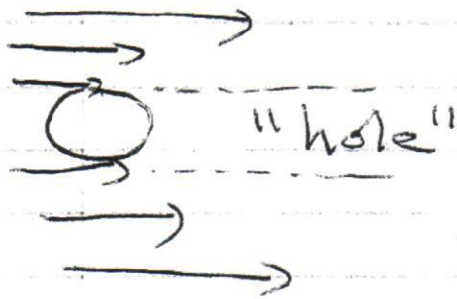


$\vec{v}$  opposite

$\vec{u}$  i.e. ~~reverse~~

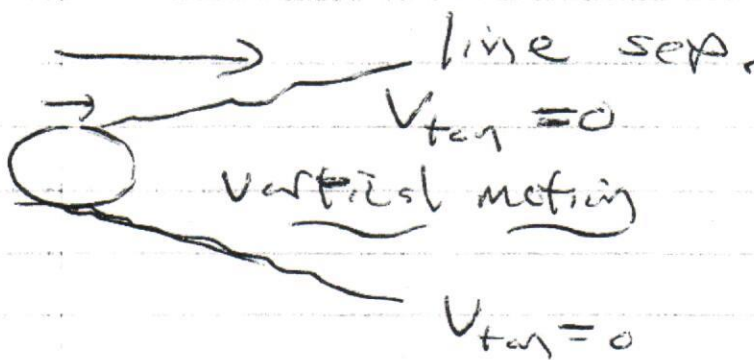
$\left\{ \begin{array}{l} u > 0 \\ v < 0 \end{array} \right.$

- origin of wake is no-slip  
 b.c. + { viscosity, turbulence } after separation



but flow is unstable!

$\infty$



$$\underline{\omega} = \nabla \times \underline{V} \neq 0$$

- boundary of wake traced by fluid particles:

→ passing close to body

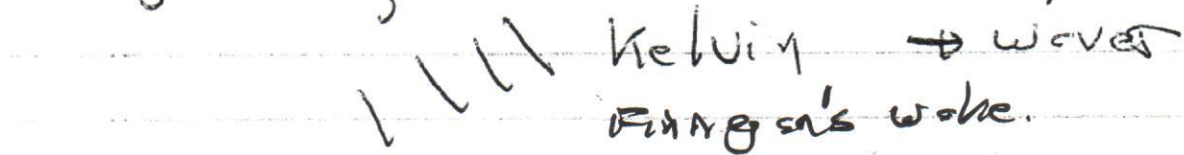
→ scattered by diffusion and turbulent mixing

→ expansion



Notes:

- in general, wake multi-component



S.S.  
Fung's

Kelvin

due: screw  
bubbles  
k.c.  
(skin  
friction)

- here, consider spherical cow  
of wake problems

→  $\rho, v$

→  sphere.

so  $F_d \sim \rho U^2 R^2 f(R_e)$

→  $\Rightarrow$  no surface effects.

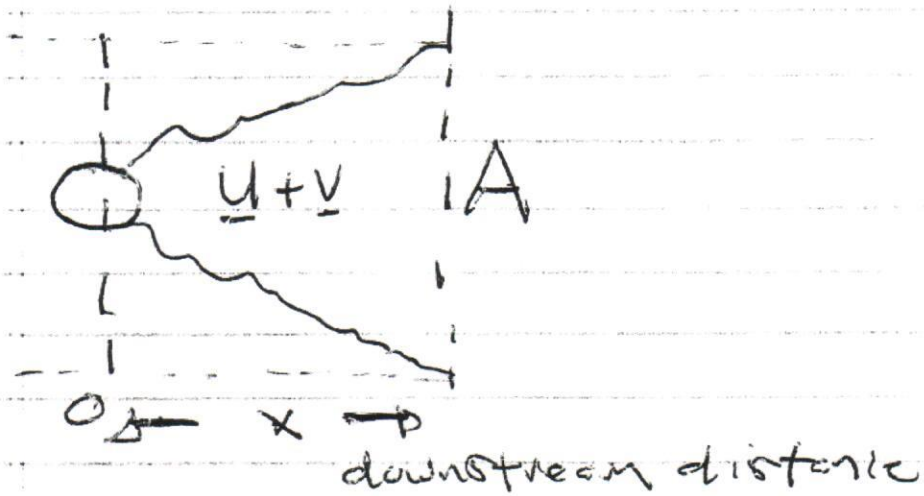
↳

→ How calculate wake structure?

Force of Drag  $\equiv$  Rate of Net Momentum Loss from Flow



i.e.

Rate Momentum Loss  $\equiv$ 

$$A \rho_{\text{total}}(x) - A \rho_{\text{Tot}}(0) = F_d$$

$$\rho_{\text{Tot}}(0) \equiv \rho + \rho U^2/2$$

total head.

$$\rho_{\text{Tot}}(x) \equiv \rho + \rho(U+V)^2/2$$

$$A \sim \pi w(x)^2$$

$w \equiv$  width of wake at  $x$  downstream

$$\therefore F_d \approx w(x)^2 \left[ \left( \rho + \frac{\rho(U+V)^2}{2} \right) - \left( \rho + \frac{\rho U^2}{2} \right) \right]$$

$\rho$  unchanged  $\rightarrow$   
w/out straight streamlines

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$$F_d \sim w(x)^2 \left[ \cancel{\rho} + \frac{\cancel{\rho} u^2}{2} + \frac{2 \cancel{\rho} u v_x}{2} - \cancel{\rho} - \frac{\cancel{\rho} u^2}{2} \right]$$

$$\sim \rho u v_x w(x)^2$$

n.b. why  $\rho(x) \sim \rho(x)$  ?

$$F_d \sim \rho u v_x w(x)^2$$

Now, need  $w(x)$  to get  $v_x$  ↓

→ Observe:

- problem now reduced to one of scale
- wakes are self-similar!

$$\Rightarrow w \sim x^\alpha, \quad \alpha ?$$

- wakes can be laminar or turbulent.

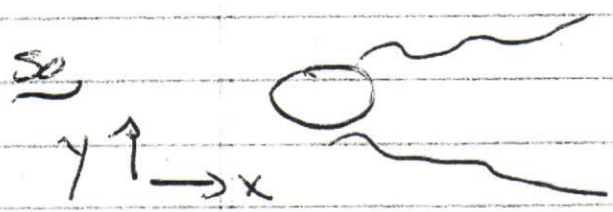
i.) Laminar

$UR/\nu < 1$

now  $\frac{\partial \underline{v}}{\partial t} + \underline{v} \cdot \nabla \underline{v} - \nu \nabla^2 \underline{v} = -\frac{\nabla p}{\rho}$

st. state

$\underline{v} \cdot \nabla \underline{v} + \underline{v} \frac{\partial \underline{v}}{\partial x} - \nu \nabla^2 \underline{v} = -\frac{\nabla p}{\rho}$



$\nabla \cdot \underline{v} = 0$

$u \frac{\partial v_y}{\partial x} - \nu (\frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial y^2}) v_y = -\frac{\partial p}{\partial y}$

and

$u \frac{\partial v_x}{\partial x} - \nu \frac{\partial^2 v_x}{\partial y^2} = -\frac{\partial p}{\partial x}$

take  $\frac{\partial}{\partial x} \sim 1/x$

$\frac{\partial}{\partial y} \sim 1/w$



$$\left(\frac{U}{x} - \frac{\nu}{W^2}\right) U_y \sim -\frac{\rho}{W^2}$$

$$\left(\frac{U}{x} - \frac{\nu}{W^2}\right) U_x \sim -\frac{\rho}{x\rho}$$

$$\nabla \cdot \underline{V} = 0 \Rightarrow \frac{U_x}{x} \sim \frac{U_y}{W}$$

as  $\rho$  negligible (will show)  $\Rightarrow$

$$\frac{U}{x} \sim \frac{\nu}{W^2}$$

$$\Rightarrow \boxed{W \sim (\nu x / U)^{1/2}}$$

$\rightarrow$  diffusive spreading of momentum, by  $\nu$

$\rightarrow \sim (\nu t)^{1/2}$   
with  $t \sim x/U$ .



100  
 $w \sim \left(\frac{x}{R}\right)^{1/2} \left(\frac{vCR}{u}\right)^{1/2}$

$w/R \sim \left(\frac{x}{R}\right)^{1/2} / Re^{1/2}$

$v_x \sim \frac{\sqrt{v d}}{\rho u w^2}$

→ skin Blasius B.L. thickness.

→ in case you are wondering:

$\rho \sim \frac{v v_y}{w^2}$  (if assume)

and

$\frac{v_x}{x} \sim \frac{v_y}{w}$

$\rho \sim \rho r v_x / x$

and  $\rho / \rho_x \sim \frac{r v_x}{x^2} \ll \frac{r v_x}{w^2}$

drop  $\rho$ .

and safely  $r v_y / w^2$

(ii) Turbulent

$$Re \sim UR/\nu \gg 1$$

$$\underline{u} \cdot \nabla \underline{u} + \underline{v} \cdot \nabla \underline{u} - \cancel{\nu \nabla^2 \underline{u}} = -\frac{\nabla p}{\rho}$$

$$\Rightarrow \frac{u}{x} v_x \sim \frac{\tilde{v}_y}{W} v_x$$

ignore

$\int$   
wave spreads  
by advection, not diffusion

$\tilde{v}_y \sim$  turbulent velocity

$$W \sim \frac{\tilde{v}_y x}{l}$$

Take wake turbulence isotropic;

so  $\tilde{v}_x \sim \tilde{v}_y$

Fair?  
Test?

$$W \sim x \tilde{v}_x / U$$

but from drag:

$$\tilde{v}_x \sim F_d / \rho y W^2$$

$\Rightarrow$



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$$W \sim x \frac{F_d}{\rho u^2 w^2} \sim x \left( F_d / \rho u^2 w^2 \right)$$

$$W^3 \sim F_d x / \rho u^2$$

$$\Rightarrow W \sim \left( F_d / \rho u^2 \right)^{1/3} x^{1/3}$$

$$\sim \left( C_D R^2 \right)^{1/3} x^{1/3}$$

then, comparing widths:

laminar:  $w/R \sim (x/R)^{1/2} Re^{-3/2}$   
 $Re \sim UR/\nu$

turbulent:  $w/R \sim (x/R)^{1/3} C_D^{1/3}$

interestingly, Laminar wake expands  
 with downstream length more  
 rapidly ↓

Why?

→ turbulence can relax  $\Delta V$  behind object (due separation) rapidly, and faster than  $v$ . Thus surrounding flow penetrates the dead water region more rapidly.

Also observe: Wake  $Re$  drops with

$x$

→

$$Re \sim \frac{w v_y}{\nu} \sim \frac{w v_x}{\nu} \sim \frac{w}{\nu} \frac{F_d}{\rho U W}$$

$\uparrow$   
y direction (opp)  
 $\uparrow$  Wake flow  $Re$

$$Re \sim F_d / \rho U W \nu$$

$$\sim U^2 R^2 \rho C_D$$

$$\sqrt{\rho U^2 (C_D R^2)^{1/3} x^{1/3}}$$

$$C_D \sim 1$$

$$\sim \left( \frac{UR}{\nu} \right) \left( \frac{R}{x} \right)^{1/3}$$



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$$Re(x) \sim Re_0 (R/x)^{1/3}$$

and  $Re(x) \rightarrow 0$  at

$$x_L \sim R (Re_0)^3$$

distance behind boat where  
turbulent wake transitions to  
laminar.

i.e. skin  $l_d$ : transition from turbulent  
mixing to viscous mixing

N.B. In wake, vertical/rotational region  
can expand into irrotational  
region, but never reverse!

i.e. would really violate H-Thm...

## Wakes - Supplement

Shear

→ Revisit turbulent wake using turbulent viscosity, i.e.

$$W \sim (rx/\mu)^{1/2} \quad (r \rightarrow D_T)$$

$$\rightarrow (D_T x / \mu)^{1/2}$$

i.e. is width of turbulent wake set by turbulent diff. following Blasius Law.

but  $D_T \sim W \tilde{\nu} \Rightarrow$  turbulent viscosity at mixing length level.

$$\sim W (\bar{F}_d / \rho U W^2)$$

$$\sim F_d / \rho U W \sim \text{const} / W$$

⇒

$$W \sim (F_d x / \rho U^2 W)^{1/2}$$

$$W^{3/2} \sim (F_d / \rho U^2)^{1/2} x^{1/2} \sim (C_D R^2)^{1/2} x^{1/2}$$

$$W \sim (C_D)^{1/3} R^{2/3} x^{1/3} \sim C_D^{1/2} R x^{1/2}$$



$$\Rightarrow \boxed{w/R \sim c_D^{1/3} (x/R)^{1/3}}$$

explains ✓

$$\text{Now, } D_T \sim \tilde{\nu} w$$

$$\sim \frac{(\tilde{\nu} w^2)}{w}$$

$$\sim \frac{\rho U \tilde{\nu} w^2}{\rho U w}$$

$$\sim \frac{Q}{w} \sim \frac{Q}{R} (x/R)^{1/3}$$

r". - Point is that turbulent viscosity mixing drops downstream, relative to constant viscous mixing.

- follows from  $\tilde{\nu} w \sim \frac{Q}{w}$   $\xrightarrow{\text{const.}}$

- explains why turbulent wake spreads more slowly than laminar wake.

→ Some Observations re: Wake Flows

→ note,

$$F_x = -\rho U \int_{\text{wake}} v_x dy dz$$

Now  $Q = \rho \int v_x dy dz$

↓  
mass flow due to  $v_x$   
⇒ deficit.

→ but if encircle body



$$\rho \int \underline{v} \cdot d\underline{a} = 0 \quad \text{c.e. continuity!}$$

Now total  $\underline{v} \rightarrow$  { velocity field  
departure from  $\underline{U}$   
= vertical  
Wake flow + potential  
Flow



so, must have  $\nabla \cdot \mathbf{v} = 0$  s/t  
Flow

$$\int \nabla \cdot \mathbf{v} \, d\mathbf{a} = Q/\rho$$

then, for area at  $r$ :

$$v \pi r^2 \sim Q/\rho$$

$$\Rightarrow v \sim Q/r^2$$

$$\phi \sim Q/r$$

} global adjustment  
in potential flow  
due wake/viscosity  
(localized)

Message:

A little  $r$  forces a  
global adjustment in  
flow structure.